

1 An experimental study of the solubility and speciation of MoO₃(s) in
2 hydrothermal fluids at temperatures up to 350 °C

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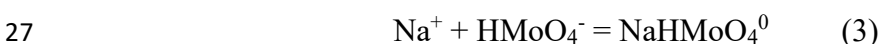
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Abstract

13 The solubility of molybdenum trioxide (MoO₃(s)) in aqueous solutions has been
14 investigated experimentally at 250, 300 and 350 °C and saturated water vapor pressure,
15 and total Na concentrations ranging from 0 to 3 m. Results of these experiments show
16 that the solubility of MoO₃(s) increases with increasing temperature and at 350 °C can
17 reach several thousand ppm at high salinity (> 1 m NaCl). At low Na⁺ activity, MoO₃(s)
18 dissolves dominantly as HMoO₄⁻, whereas at high Na⁺ activity, the dominant species is
19 NaHMoO₄⁰. The two dissolution reactions are:



22 The values of the logarithms of the equilibrium constants for Reaction 1 are $-5.20 \pm$
23 0.12 , -5.31 ± 0.17 and -5.50 ± 0.09 at 250, 300 and 350 °C respectively, and for Reaction
24 2 are -3.40 ± 0.11 , -3.25 ± 0.19 and -2.97 ± 0.09 for the same temperatures. In
25 combination, these equilibrium constants yield equilibrium constants for the reaction
26 relating the two aqueous species,



28 The values of the logarithms of the equilibrium constants for Reaction 3 are 1.80 ± 0.16 ,
29 2.06 ± 0.25 and 2.53 ± 0.13 at 250, 300 and 350 °C, respectively. Calculations, based
30 on the results of this study and thermodynamic data available for other species, suggest

31 strongly that in ore-forming hydrothermal systems, molybdenum is transported mainly
32 as NaHMoO₄⁰ and deposits as molybdenite in response to cooling and possibly a
33 reduction in *f*O₂.

34

35

Introduction

36 Molybdenum is a rare element with a very low abundance of 1.1 ppm in the
37 upper continental crust and an even lower abundance in the mantle (50 ppb)
38 (McDonough and Sun, 1995; Rudnick and Gao, 2003). Despite this, molybdenum may
39 be concentrated by hydrothermal fluids to levels in excess of 0.1 wt.% Mo (Ulrich and
40 Mavrogenes, 2008; Zhang et al., 2012; Audétat and Li., 2017), which is sufficient for
41 economic exploitation. Indeed, the global resources of molybdenum are entirely the
42 products of such concentration, mostly in the form of porphyry Mo and Cu-Mo deposits
43 that develop from hydrothermal fluids exsolved from felsic magmas (Mutschler et al.,
44 1999; Zeng et al., 2013; Zhang et al., 2014; Audétat and Li., 2017).

45 Previous studies investigating the solubility and speciation of molybdenum in
46 hydrothermal fluids have generally concluded that the Mo is transported mainly in the
47 6+ state as molybdic acid (H₂MoO₄) and its dissociation products HMoO₄⁻ and MoO₄²⁻
48 (Candela and Holland, 1984; Wood et al., 1987; Keppler and Wyllie, 1991; Minubayeva
49 and Seward, 2010). Among these species, HMoO₄⁻ is predicted to dominate Mo
50 transport, except at low temperature, for which H₂MoO₄⁰ and MoO₄²⁻ also play a role
51 at acidic and near-neutral to alkaline conditions, respectively (Ivanova, 1975; Kudrin,
52 1985; Wood et al., 1987; Minubayeva and Seward, 2010; Dadze et al., 2014, 2017a;
53 Williams-Jones and Migdisov, 2014). The high salinity (> 1 m NaCl) of the fluids
54 interpreted to be responsible for the formation of porphyry Mo and Cu-Mo deposits
55 (Audétat and Li., 2017), however, suggests that species involving Na and/or Cl may
56 also play a role in molybdenum transport. Recognizing this possibility, a number of
57 studies have investigated the effect of salinity (NaCl) on molybdenum solubility (e.g.,
58 Kudrin, 1989; Cao 1989; Ulrich and Mavrogenes, 2008; Bali et al., 2012; Zhang et al.,
59 2012, Tattitch and Blundy 2017; Dadze et al., 2018). Although these studies have

60 proposed species involving Na, e.g., NaHMoO₄⁰ (Kudrin, 1989; Cao,1989), or Cl, e.g.,
61 MoO_mCl_n^{6-2m-n} (Ulrich and Mavrogenes, 2008; Borg et al., 2012), to our knowledge,
62 only Kudrin (1989) and Cao (1989) have reported equilibrium constants for reactions
63 involving these species.

64 In view of the limited data available on the speciation of Mo in NaCl-bearing fluids
65 and their potential importance in the genesis of hydrothermal Mo deposits, we
66 conducted a series of experiments in order to quantitatively evaluate this speciation
67 Here, we report the results of experiments designed to determine the solubility of
68 molybdenum trioxide in aqueous fluids as a function of salinity and pH at temperatures
69 up to 350 °C. The data are used to evaluate the aqueous speciation of molybdenum at
70 the different conditions and determine the equilibrium constants for reactions involving
71 the dominant species. Using these constants, we then address the question of whether
72 species other than molybdic acid and its dissociation products could play a significant
73 role in the transport of molybdenum in ore-forming hydrothermal systems.

74

75

Methods

76 The solubility of MoO₃(s) in NaCl-bearing aqueous solutions was investigated
77 experimentally at 250, 300 and 350 °C and vapor-saturated water pressure. This
78 involved dissolving MoO₃(s) obtained from Alfa Aesar (99.999% pure) in a series of
79 batch solutions with variable pH and salinity that were prepared for the purpose. The
80 solubility of MoO₃(s) in these solutions and its dependence on salinity and pH were
81 then determined and used to evaluate the solubility product of MoO₃(s) and the stability
82 constants of reactions involving the dominant molybdenum species. As experiments
83 involving NaCl do not allow us to readily separate the effects of complexes involving
84 Na from those involving Cl, we also evaluated the solubility of MoO₃(s) in sodium-
85 triflate (NaCF₃SO₃) aqueous solutions. As the triflate ion is non-complexing, i.e.,
86 interactions between this ion and metals like Mo⁶⁺ are extremely weak (Fabes and
87 Swaddle, 1975; Palmer and Drummond, 1988; Applegarth et al., 2015), any increase in
88 Mo concentration with increasing concentration of sodium triflate can be attributed to

89 ion-pairing of HMoO₄⁻ or MoO₄²⁻ with Na⁺. However, although the triflate ion is stable
90 to temperatures > 400 °C in solutions with near neutral pH, it begins to decompose at
91 temperatures above 280 °C in highly acidic solutions (Applegarth et al., 2015). Our
92 experiments with sodium-triflate solutions were therefore limited to the 250 °C
93 isotherm.

94 The experimental method used in this study is similar to that of previous studies
95 in our laboratory (e.g., Migdisov and Williams-Jones, 2005; Timofeev et al., 2018),
96 Prior to the experiments, the solid (MoO₃(s)) was introduced into a short silica-glass
97 holder capped with quartz wool to serve as a barrier preventing the solid from entering
98 the autoclaves directly but permitting interaction between the solid and the solution
99 during the experiments. In order to ensure that oxygen fugacity remained high enough
100 to preclude formation of Mo(IV) species, a second silica glass, quartz wool-capped
101 holder containing the oxygen buffer Mn₂O₃(s)/Mn₃O₄(s) was prepared; the oxygen
102 fugacity in equilibrium with this buffer greatly exceeds the oxygen fugacity of the
103 MoO₃(s)/MoO₂(s) transition (Robie and Hemingway, 1995). The two holders and 15 -
104 20 ml of the experimental solution were placed in a titanium autoclave (grade 2 ASTM
105 B348). The holders were designed such that during the experiments, the top of the
106 holder containing the buffer was well above the vapor/liquid interface, whereas the
107 holder containing the MoO₃(s) was immersed in liquid (Fig. 1).

108 The autoclaves were heated in a Fisher Forced draft oven inside an aluminum box
109 with 1.5 cm thick walls to minimize temperature gradients. The thermal gradient in this
110 system was determined to be < 1 °C for the entire height of the oven (45cm) by Migdisov
111 and Williams-Jones (2007). The duration of experiments was 7 - 10 days, which has
112 been shown to be sufficient to ensure a steady-state solubility for experiments involving
113 Mo (Rempel et al., 2006, Hurtig and Williams-Jones, 2014). After each experiment, the
114 autoclaves were quenched to room temperature in cold water and opened, and the
115 holders containing MoO₃(s) and the oxygen buffer were removed. A 2 ml aliquot of
116 solution was withdrawn from each autoclave and used to determine the pH. This was
117 followed by the addition to each autoclave of a 3 ml aliquot of a solution containing
118 equal proportions of nitric acid, hydrochloric acid and nano-pure water to dissolve any

119 Mo-bearing precipitates that might have formed on the walls of the autoclaves during
120 quenching. The resulting solutions were removed from the autoclaves after 30 minutes,
121 diluted and then analyzed for their molybdenum concentration using Inductively
122 Coupled Plasma Mass Spectrometry (ICP-MS). After the experiments, the MoO₃ solid
123 and buffer were analyzed by X-ray diffraction to confirm that other solids had not
124 formed during the experiments. No additional solids were detected, indicating that the
125 solubility measured in this study corresponded only to the dissolution of MoO₃(s) and
126 that the buffer had behaved as expected.

127 The pH at the temperature of the experiments (pH_T) was extrapolated from the
128 pH measured in the experimental solutions after quenching (pH_{25°C}). This was done
129 using the modified extended Debye-Hückel equation for NaCl-dominated solutions
130 (Helgeson et al., 1981; Oelkers and Helgeson., 1990; Oelkers and Helgeson, 1991):

$$131 \quad \log \gamma_n = -\frac{A \cdot [z_i]^2 \cdot \sqrt{I}}{1 + B \cdot \hat{a} \cdot \sqrt{I}} + b_\gamma \cdot I + \Gamma \quad (4)$$

132 in which A and B are the Debye-Hückel solvent parameters, \hat{a} the distance of closest
133 approach of an ion i, which is specific to the ion of interest, z the charge of the ion, b_γ
134 the extended parameter for NaCl, Γ a molarity to molality conversion factor, and I the
135 true ionic strength after consideration of all dissolved species.

136

137 **Results**

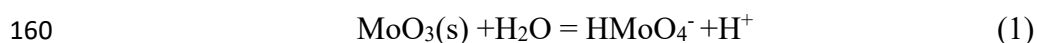
138 *Identification of dissolved molybdenum species*

139 The results of the experiments at 250, 300 and 350 °C are reported in Table 1. In
140 order to evaluate the relationship between the pH, NaCl concentration and molybdenum
141 solubility, and the stoichiometry of the dominant Mo species, the logarithms of the
142 concentrations of Mo measured in the experimental solutions were plotted as a function
143 of the logarithms of the NaCl concentration (Fig. 2a–c) and pH_T (Fig. 3). From Figure
144 2, it is evident that for NaCl concentrations ≥ 0.01 m, the concentration of Mo increases
145 linearly (~1:1 slope) with the concentration of NaCl for each of the isotherms; for
146 experiments conducted at 300 and 350 °C, the concentration of Mo in the NaCl-free
147 solutions is very similar to that in solutions containing 0.1 m NaCl. The concentration

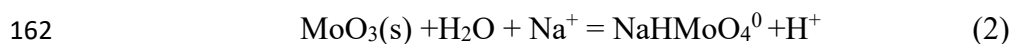
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148 of Mo in the sodium triflate solutions also increases linearly with sodium triflate
149 molality and does so along the ~1:1 trend produced by the experiments with the NaCl
150 solutions (Fig 2a). This supports the hypothesis that, if the relationship between Mo and
151 NaCl concentration reflects complexation, the resulting species involved Na and not Cl.
152 Finally, we note that the concentration of Mo increases with pH_T in a ratio of log mMo
153 to pH that is close to unity (Fig. 3).

154 Based on the approximately 1:1 dependence of the logarithm of Mo solubility
155 on the logarithm of NaCl concentration and pH, for NaCl concentrations ≥ 0.1 m NaCl,
156 and its independence from NaCl concentration at lower concentrations of the latter, we
157 interpret the solubility of Mo to have been controlled by the formation of two aqueous
158 molybdate species. One of these species is HMoO₄⁻, which formed as a result of the
159 reaction:



161 The other species is NaHMoO₄⁰, which formed through the reaction:



163

164 *Calculation of ion activity and derivation of stability constants*

165 As discussed above, HMoO₄⁻ and NaHMoO₄ were identified as the two dominant
166 Mo species in the experimental solutions. At low salinity, HMoO₄⁻ was the dominant
167 species, whereas NaHMoO₄ was dominant at high salinity. The activity of each of the
168 dissolved species and the equilibrium constants for Reactions (1) and (2) were
169 calculated using the methods described in previous publications by our group (e.g.,
170 Nisbet et al., 2018; Timofeev et al., 2018; Wang et al., 2019). The standard Gibbs free
171 energy of the aqueous species HMoO₄⁻ and NaHMoO₄ were determined iteratively for
172 each of the isothermal solubility series of experiments using the program Optima,
173 which is part of the HCh package (Shvarov, 2010 and 2015). This program determines
174 the Gibbs free energy of species by minimizing the sum of squared deviations of the
175 experimentally determined concentrations of the species from the calculated
176 concentrations using the equilibrium composition of the solution.

177 We considered the following species in our model, H₂O, H⁺, OH⁻, Na⁺, NaOH, NaCl,
178 Cl⁻, HCl, MoO₃(s), HMoO₄⁻ and NaHMoO₄ and determined the standard Gibbs free
179 energy of the two molybdenum species from the molality of Mo, NaCl and HCl for
180 each experiment. The molality of HCl was calculated from the starting NaCl
181 concentration and the pH measured after each experiment, which was extrapolated to
182 the experimental temperature using the modified extended Debye-Hückel equation (see
183 Methods). In order to ensure that the solution was saturated with respect to MoO₃(s),
184 an excess amount of this solid was stipulated during the running of OptimA. Excess
185 amounts of the oxygen buffer assemblage were also stipulated. The Haar-Gallagher-
186 Kell (Kestin et al., 1984) and Marshall and Franck (1981) models were used to
187 determine the thermodynamic properties and dissociation constant of H₂O for the
188 experimental conditions. Thermodynamic data for Cl⁻ were taken from Johnson et al.
189 (1992), for H⁺ from Wesolowski et al. (1984), for Na⁺ and NaOH from Shock et al.
190 (1997), for NaCl from Sverjensky et al. (1997), for HCl from Tagirov et al. (1997) and
191 for MoO₃(s), Mn₂O₃(s) and Mn₃O₄(s) from Robie and Hemingway (1995). The Gibbs
192 free energy of HMoO₄⁻ and NaHMoO₄ for each experimental temperature calculated
193 using these data and the method described above are reported in Table 2 together with
194 Gibbs free energy data for other relevant species. Formation constants for these species
195 from MoO₄²⁻, which were calculated using the Gibbs free energy data reported in Table
196 2, are reported in Table 3. The uncertainty for each of the values in these tables is that
197 calculated using the OptimA program.

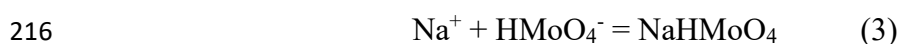
198 The formation constants for HMoO₄⁻ and NaHMoO₄ reported in Table 3 were fitted
199 to the Ryzhenko-Bryzgalin (MRB) model (Ryzhenko et al., 1985) modified by Borisov
200 and Shvarov (1992) as described in Shvarov and Bastrakov (1999). This was done using
201 the program OptimC in the HCh package (Shvarov, 2010 and 2015). The MRB model
202 was developed to fit the temperature and pressure dependence of dissociation constants
203 for ion pairs through the following equation:

204
$$\log K_{(T,P)} = \frac{T_r}{T} \log K_{(T_r,P_r)} + B_{(T,P)} \left(A_{zz/a} + \frac{B_{zz/a}}{T} \right) \quad (5)$$

205 in which K is the dissociation constant of the ion pair, T_r and P_r are the reference

206 temperature and pressure, and $A_{zz/a}$ and $B_{zz/a}$ are fitting parameters. The term $B_{(T,P)}$
207 accounts for the properties of water at temperature T and pressure P, and was evaluated
208 using the data of Marshall and Franck (1981). The values for the parameters derived
209 from this model for HMoO_4^- and NaHMoO_4 are reported in Table 4 together with
210 formation constants for these species determined by the MRB model.

211 The MRB model and the fitting parameters derived for HMoO_4^- and NaHMoO_4
212 were then used to calculate equilibrium constants (log K) for Reactions (1) and (2) at
213 each temperature investigated experimentally. These constants are reported in Table 5.
214 Reactions 1 and 2 and the corresponding constants, in turn, were combined to yield
215 equilibrium constants for the reaction relating the two aqueous species:



217 The equilibrium constants for this reaction are also reported in Table 5. Uncertainties
218 associated with the calculation of the equilibrium constants were estimated from the
219 deviation of the measured constants from those obtained using the Gibbs free energy
220 determined by OptimA and optimized using OptimC.

221

222 Discussion

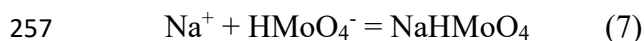
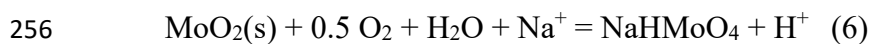
223 *Molybdenum speciation*

224 The results of our experiments show that both HMoO_4^- and NaHMoO_4 contribute
225 to the solubility of $\text{MoO}_3(\text{s})$ in NaCl-bearing aqueous solutions at elevated temperature.
226 We illustrate this in Figure 4, which shows the log activity of the two species
227 (determined using OptimA) as a function of the log activity of Na at 250, 300 and
228 350 °C for a pH of 2.1. Also shown is the logarithm of the total Mo activity. From this
229 figure, it is evident that at very low activity of Na^+ , the solubility of $\text{MoO}_3(\text{s})$ is
230 controlled mainly by HMoO_4^- but that even at a Na^+ activity as low 0.02, NaHMoO_4 is
231 the dominant aqueous Mo species; at a Na^+ activity above 0.05 the contribution of
232 HMoO_4^- is negligible. The importance of NaHMoO_4 also increases with increasing
233 temperature as illustrated in Figure 5, where it can be seen that the predominance
234 boundary for NaHMoO_4 moves to lower activity of Na^+ with increasing temperature.

235 Thus, at 250 °C, approximately 75% of the Mo is dissolved as NaHMoO₄, if the salinity
236 is 0.1m, whereas this proportion increases to > 90% at 350 °C for the same salinity.
237 This behaviour may reflect the fact that the dominant species is neutral, which is
238 consistent with the observation that, with increasing temperature, the dielectric constant
239 of water decreases and its hydrogen bonding network weakens considerably, thereby
240 favouring aqueous species of low or no charge (Fernández et al.,1997).

241 *Comparison to previous studies*

242 From the results of our experiments, it is clear that the solubility of MoO₃(s) is
243 higher in NaCl-bearing than in NaCl-free aqueous solutions at elevated temperature.
244 The same conclusion has been reached by most previous experimental studies that have
245 investigated the solubility of MoO₃(s) (and MoO₂(s)) in NaCl-bearing and NaCl-free
246 aqueous solutions (Kudrin, 1989; Cao 1989; Ulrich and Mavrogenes, 2008; Bali et al.,
247 2012 ; Zhang et al., 2012 and Dadze et al., 2018). Opinion, however, is divided over
248 whether the higher solubility of Mo in NaCl-bearing aqueous solutions is due to the
249 formation of Na-bearing Mo species (Kudrin, 1989; Cao 1989; Bali et al., 2012), the
250 formation of Cl-bearing Mo species (Ulrich and Mavrogenes, 2008; Dadze et al., 2018)
251 or is simply an artifact of the increased ionic strength of the solution due to the presence
252 of Na⁺ and Cl⁻ (Dadze et al., 2017b). To our knowledge, only Kudrin (1989) has
253 reported stability constants for reactions involving Mo species other than molybdic acid
254 and its dissociation products at elevated temperature. He reported stability constants for
255 the reactions:



258 at temperatures between 300 and 450 °C and 500 bar.

259 In order to compare the results of our experiments with those of Kudrin (1989),
260 which investigated the solubility of MoO₂(s) rather than MoO₃(s) (this study), we based
261 the comparison on Reaction 3. As the pressure employed in the experiments of Kudrin
262 (1989) was 500 bar, the comparison also required correcting for the fact that our
263 experiments were conducted at saturated vapor pressure. We therefore extrapolated our

264 stability constants to 500 bar using the MRB model. In Figure 6, we compare the
265 equilibrium constants derived for Reaction 3 in our study with those derived from
266 Kudrin (1989). From this figure, it is evident that the results of our study are in excellent
267 agreement with those of Kudrin (1989) at 300 and 350 °C.

268 *Application to natural systems*

269 As discussed in the introduction of this paper, most of the World's supply of Mo
270 is from porphyry Mo and porphyry Cu-Mo deposits, in which the molybdenum
271 precipitated from magmatic-hydrothermal fluids (e.g., Westra and Keith.,1981;
272 Seedorff et al., 2005; Klemm et al., 2007, 2008; Audétat and Li., 2017). Therefore,
273 the results of our study would be of most relevance, if they could be applied to
274 porphyry Mo and Cu-Mo ore-forming systems. On the basis of fluid inclusion studies
275 for Climax-type deposits, the fluids exsolved from the magmas are interpreted to have
276 contained between 5 and 15 wt% NaCl_{equiv.} (Audétat and Li., 2017), and to have had
277 a total sulfur content of 0.003 m (Audétat., 2015). The pH is generally interpreted to
278 have been buffered by the mineral assemblage, muscovite-K-feldspar-quartz
279 (Seedorff et al., 2005) and oxygen fugacity to have been between 2 and 3.5 log units
280 above the fayalite-magnetite-quartz buffer (QFM) (Qiu et al., 2013; Audétat., 2015).
281 Ore formation is typically considered to have taken place at temperatures between
282 500 and 300 °C (Seedorf et al., 2005; Klemm et al., 2008; Audétat, 2015)

283 In order to test the applicability of the results of this study to porphyry Mo
284 systems, we modelled the solubility of molybdenite in an ore-forming magmatic fluid,
285 which had a salinity ranging from 1 m NaCl (~ 6 wt.% NaCl) to 3 m NaCl (~18 wt.%
286 NaCl), and cooled from 500 to 300 °C at 1000 bar (this pressure, which could reflect
287 that for a fluid evolving in a deep porphyry, was chosen to avoid phase separation
288 after exsolution from the magma). The sulfur concentration (ΣS) was assumed to be
289 0.003 m (Audétat., 2015), the pH to have been buffered by the mineral assemblage
290 muscovite-K-feldspar-quartz and fO_2 to have corresponded to 2.2 log units above
291 FMQ. These conditions are the same as those that have been estimated for the Climax
292 porphyry Mo ore-forming system (Audétat, 2015).

293 In Figure 7, we illustrate the solubility of molybdenite in the above fluid as a
294 function of temperature and salinity. At 500 °C, the concentration increases from ~
295 30 to 206 ppm as salinity increases from 0 to 3 m, emphasizing the important role
296 that salinity plays in promoting Mo solubility in porphyry systems. For the trapping
297 temperature (480 - 460 °C) of fluid inclusions coexisting with decrepitated melt
298 inclusions (and therefore representing the magmatic fluid) in the Climax deposit
299 (Audétat, 2015), the Mo concentration in a 2 m NaCl solution (the salinity of the
300 inclusions was ~1.8 m) is between 64 and 18 ppm. This concentration range is
301 remarkably similar to that reported by Audétat. (2015) for the above fluid inclusions
302 (60 - 5 ppm Mo).

303 Because Mo is in the 4+ state in molybdenite and is thought to be mobilized in
304 the 6+ state (Williams-Jones and Migdisov, 2014), the state considered in our
305 experiments, it follows that molybdenite deposition will be strongly influenced by
306 oxygen fugacity. In Figure 8, we show the solubility of molybdenite as a function of
307 salinity and fO_2 for a fluid at a temperature of 450 °C and a pressure of 1000 bar. The
308 sulfur concentration and the pH buffer were the same as for Figure 7. From Figure 8,
309 it is evident that a decrease in fO_2 from FMQ + 2.5 to FMQ will result in about an
310 order of magnitude decrease in solubility. The predicted concentrations of Mo in a 2
311 m NaCl solution at this temperature are 2 ppm, 22 ppm and 52 ppm for a fO_2
312 corresponding to that of FMQ, FMQ + 2.5, and FMQ + 3.5 at 450 °C.

313 In summary, the transport of Mo in hydrothermal fluids is strongly dependent
314 on salinity and temperature. As molybdenite is the only Mo ore-mineral, however, it
315 also follows that oxygen fugacity and reduced sulfur activity (not explicitly addressed)
316 will have a strong influence on whether an otherwise fertile fluid will produce an
317 economically exploitable Mo deposit.

318

319

Conclusions

320 The experimental data reported in this study show that molybdenite dissolves
321 dominantly as NaHMoO₄, except at exceptionally low salinity for which HMoO₄⁻ is the
322 dominant species. This has important implications for our understanding of the
323 transport of molybdenum in nature and particularly for models of ore formation in

324 porphyry systems, which have been based largely on an assumption that the metal is
325 transported as the species HMoO₄⁻. The overarching conclusion of the study is that
326 molybdenum transport is favored by high salinity, high temperature and high oxygen
327 fugacity, and that, in principle, any geological process leading to a decrease in the values
328 of any of these parameters could lead to molybdenum ore deposition.

329

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342

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519

520 **Figure captions**

521 Fig. 1. A sketch of the experimental set-up used in this study.

522 Fig. 2. The logarithm of Mo molality as a function of the logarithm of NaCl molality at 250, 300
523 and 350 °C (red dots) and as a function of the logarithm of NaCF₃SO₃ (sodium triflate) molality at
524 250 °C (blue diamonds). The uncertainty for each datum is less than the diameter of the symbol.

525 Fig. 3. The logarithm of Mo molality as a function of pH_T at 300 (brown) and 350 (green) °C .

526

527 Fig. 4. Values of log a Σ Mo (blue dots), log aNaHMoO₄ (red dashed line) and log aHMoO₄⁻ (green
528 dashed line) as a function of log aNa⁺ at 250 (a), 300 (b) and 350 °C (c). The values were obtained
529 from equilibrium constants for Reactions (1) and (2) calculated using OptimA, and are normalised
530 to a pH of 2.1.

531

532 Fig. 5. a) Predominance fields of HMoO₄⁻ and NaHMoO₄ as a function of temperature and log aNa⁺.
533 b – d) The distribution of Mo (VI) aqueous species as a function of log aNa⁺ at 250 °C, 300°C
534 and 350°C, respectively. The diagrams are based on data for the equilibrium constants of
535 Reaction 3.

536 Fig. 6. Equilibrium constants for Reaction 3 determined in this study (red squares), fitted to the BR
537 model (black dashed line) at P_{sat}, and corrected to 500bar (red dashed line) for comparison to
538 the constants derived from Kudrin (1989) for this pressure (blue dots).

539 Fig. 7. The concentration of Mo at molybdenite saturation and 1000 bar, as a function of temperature
540 in solutions containing 0 to 3 m NaCl, 0.5 m KCl, and 0.003 m Σ S; pH is buffered by the
541 assemblage, muscovite-K-feldspar-quartz, and fO₂ is fixed at 2.2 log units above the fayalite-
542 magnetite-quartz (FMQ + 2.2) buffer. The calculations were performed using HCh (Shvarov,

543 2008) and thermodynamic data for aqueous Mo species from this study (HMoO₄⁻ and
544 NaHMoO₄) and Shock, 1997 (H₂MoO₄ and MoO₄²⁻).

545 Fig. 8. The concentration of Mo at molybdenite saturation, 450 °C and 1000 bar, as a function of
546 oxygen fugacity in solutions containing 0 to 3 m NaCl, 0.5 m KCl, and 0.003 m ΣS; pH is
547 buffered by the assemblage, muscovite-K-feldspar-quartz. The calculations were performed
548 using HCh (Shvarov, 2008) and thermodynamic data for aqueous Mo species from this study
549 (HMoO₄⁻ and NaHMoO₄) and Shock, 1997 (H₂MoO₄ and MoO₄²⁻).

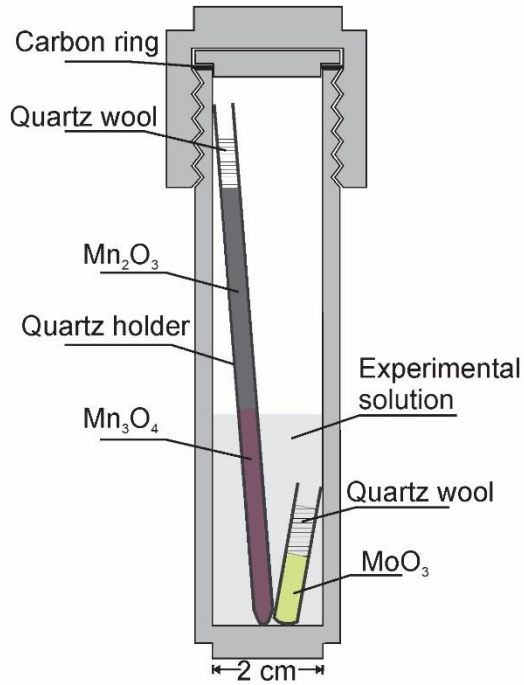


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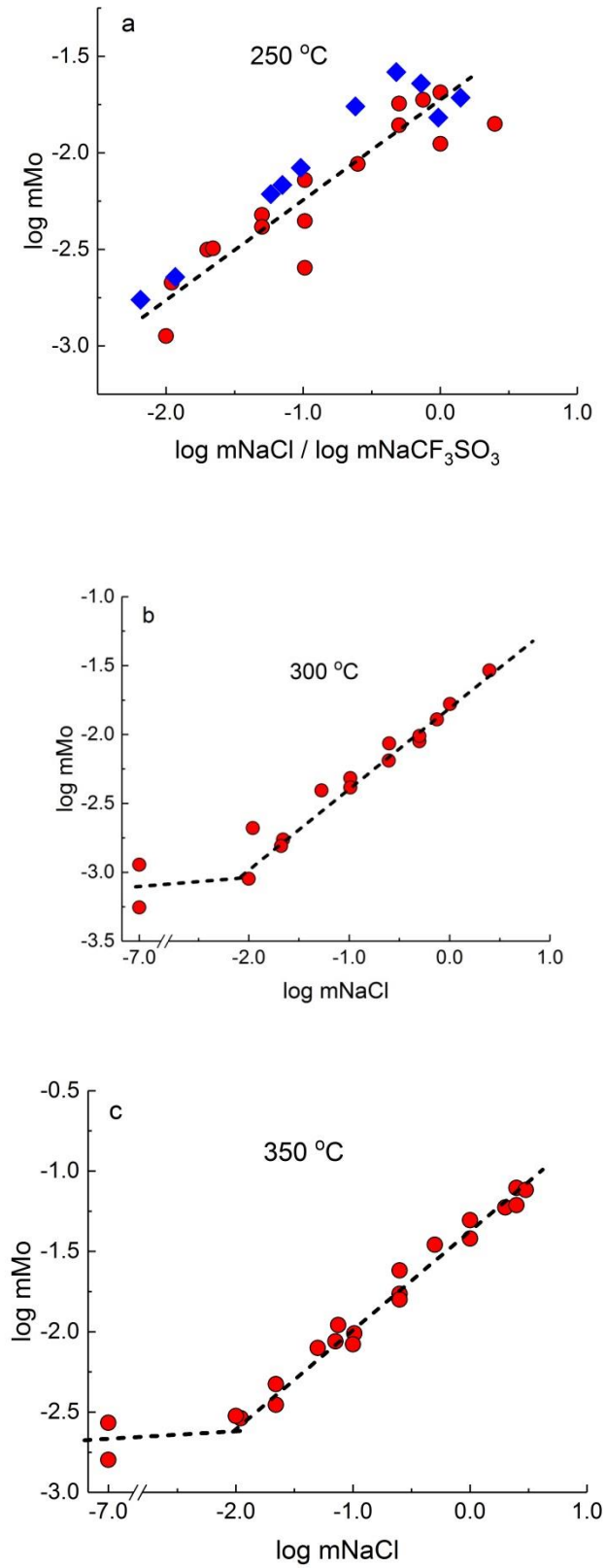


Fig. 2. The logarithm of Mo molality as a function of the logarithm of NaCl molality at 250, 300

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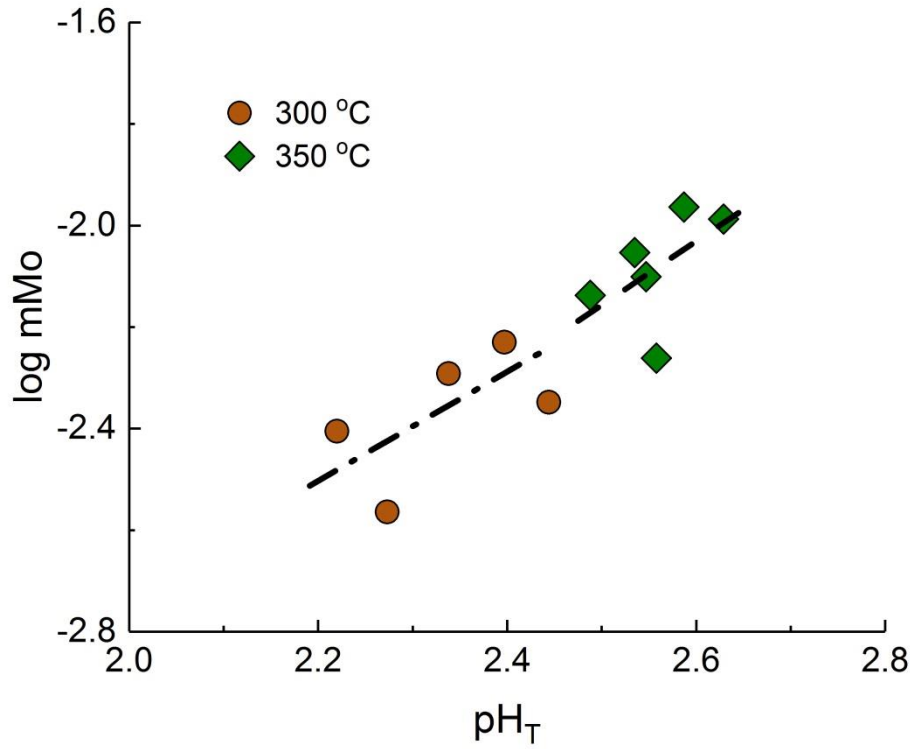


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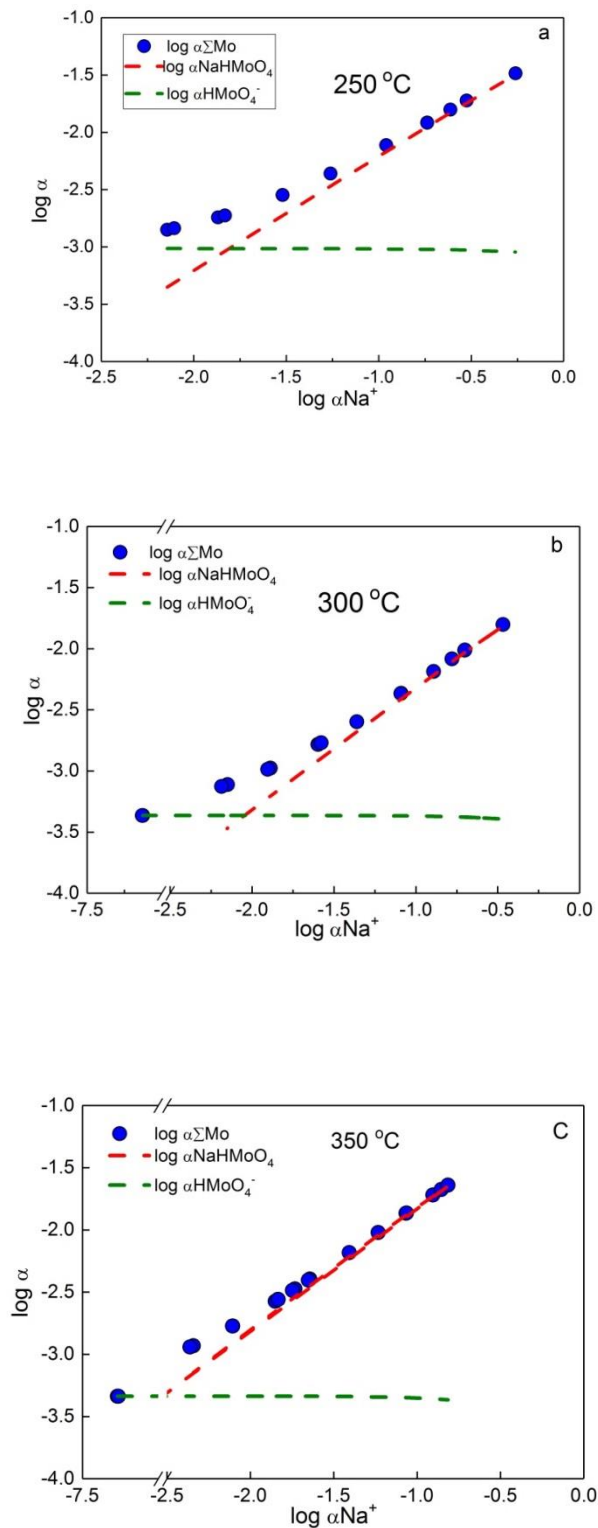


Fig. 4. Values of $\log a_{\Sigma\text{Mo}}$ (blue dots), $\log a_{\text{NaHMoO}_4}$ (red dashed line) and $\log a_{\text{HMoO}_4^-}$ (green dashed line) as a function of $\log a_{\text{Na}^+}$ at 250 (a), 300 (b) and 350 °C (c). The values were obtained from equilibrium constants for Reactions (1) and (2) calculated using OptimA, and are normalised to a pH of 2.1.

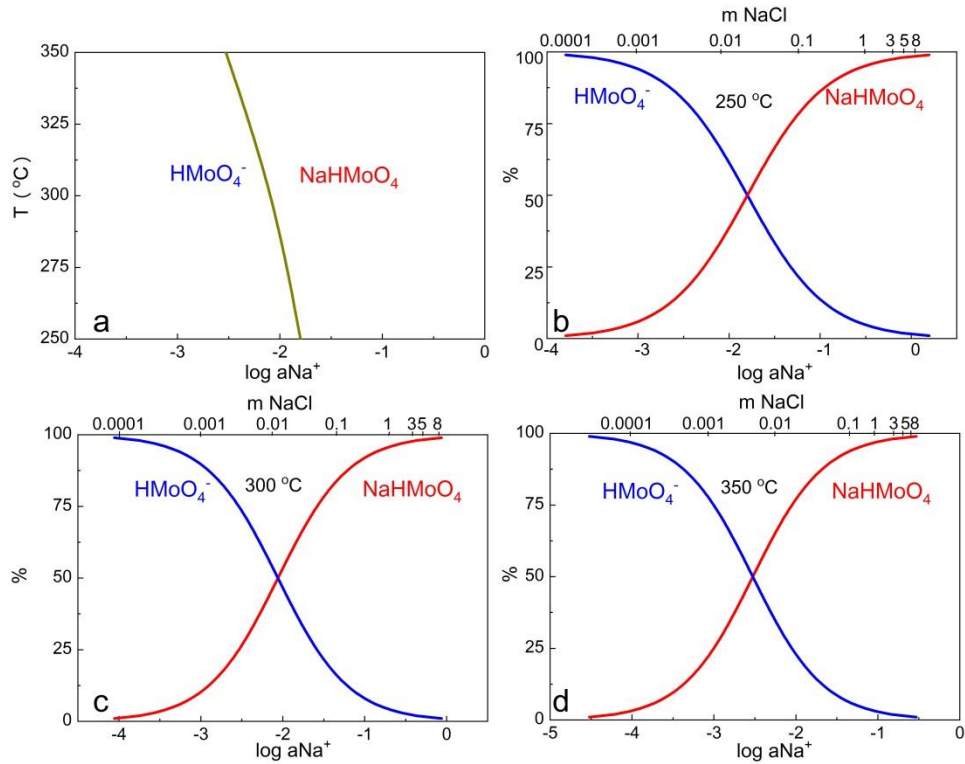


Fig. 5. a) Predominance fields of HMoO_4^- and NaHMoO_4 as a function of temperature and $\log a_{\text{Na}^+}$. b – d) The distribution of Mo (VI) aqueous species as a function of $\log a_{\text{Na}^+}$ at 250 °C, 300°C and 350°C, respectively. The diagrams are based on data for the equilibrium constants of Reaction 3.

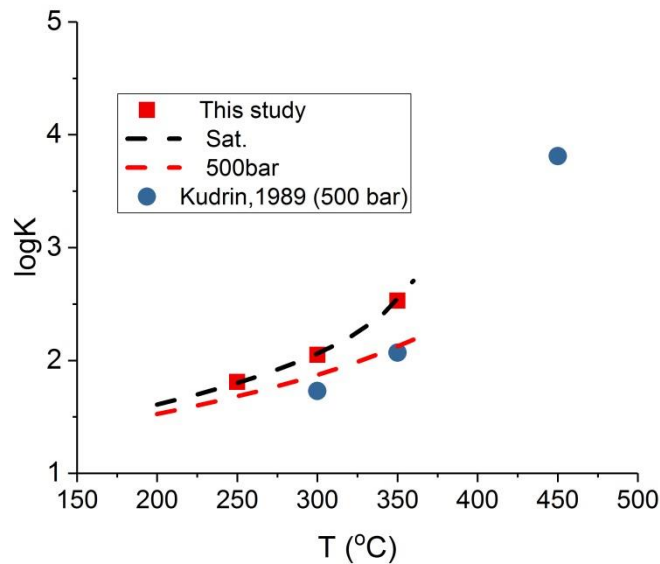


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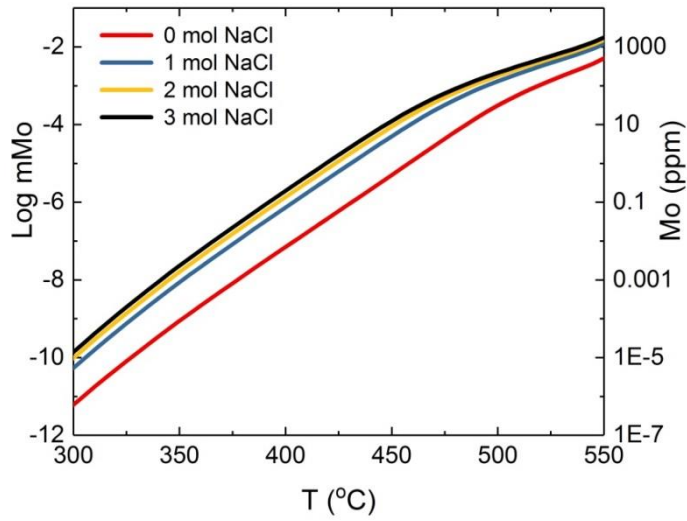


Fig. 7. The concentration of Mo at molybdenite saturation and 1000 bar, as a function of temperature in solutions containing 0 to 3 m NaCl, 0.5 m KCl, and 0.003 m Σ S; pH is buffered by the assemblage, muscovite-K-feldspar-quartz, and fO_2 is fixed at 2.2 log units above the fayalite-magnetite-quartz (FMQ + 2.2) buffer. The calculations were performed using HCh (Shvarov, 2008) and thermodynamic data for aqueous Mo species from this study ($HMoO_4^-$ and $NaHMoO_4$) and Shock, 1997 (H_2MoO_4 and MoO_4^{2-}).

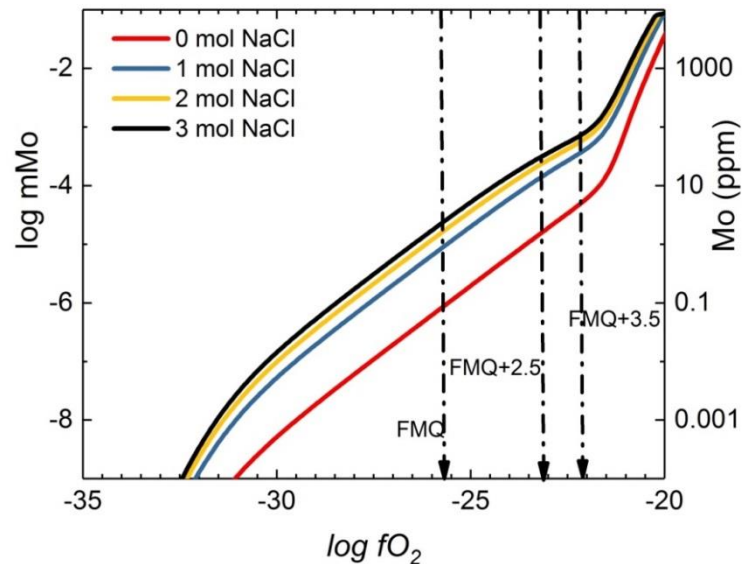


Fig. 8. The concentration of Mo at molybdenite saturation, 450 °C and 1000 bar, as a function of oxygen fugacity in solutions containing 0 to 3 m NaCl, 0.5 m KCl, and 0.003 m Σ S; pH is buffered by the assemblage, muscovite-K-feldspar-quartz. The calculations were performed using HCh

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